Appl. No. 09/975,220

REMARKS / ARGUMENTS

Claims 1 to 30 are pending in this application. The Office Action objects that the

previous reply, filed on November 21, 2002, was non-responsive because amended

claims 23, 25, 26 and 29 were not presented with their entire text underlined. This reply

presents those claims with their text completely underlined. The current reply also

indicates that the claims are amended in parentheses. The nature of the amendments

and the support for them was discussed in the previous reply filed on November 21,

2002.

With the previous reply, the applicants had also submitted a Revocation of Power of

Attorney and Statement Under 37 CFR 3.73 (b). The applicants have not received

confirmation that this revocation and statement were acknowledged. A copy of the

revocation and statement as filed on November 21, 2002, are attached to this reply. The

applicants respectfully request that this revocation and statement be acknowledged and

that the address for service be changed accordingly.

Attached hereto is a marked-up version of the changes made to the claims by the

current amendment. The attached page is captioned "Version with markings to show

changes made."

Applicants submit that the application is now in condition for allowance.

Respectfully submitted,

Mailvaganam Mahendran et al.

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VERSION WITH MARKINGS TO SHOW CHANGES MADE

In the claims:

23. (Amended) In a microfiltration membrane device, for withdrawing permeate
essentially continuously from a multi-component liquid substrate while increasing the
concentration of particulate material therein, said membrane device including:
a multiplicity of hollow fiber membranes, or fibers, unconfined in a shell of a
module, said fibers together having a surface area > 1 m ² , said fibers being swayable in
said substrate, said fibers being subject to a transmembrane pressure differential in the
range from about 0.7 kPa (0.1 psi) to about 345 kPa (50 psi), and each fiber having
length > 0.5 meter;
a first header and a second header disposed in transversely spaced-apart
relationship with said second header within said substrate;
a first header and a second header having opposed terminal end portions of
each fiber sealingly secured therein, all open ends of said fibers extending from a
permeate-discharging face of at least one header;
permeate-collection means to collect said permeate, sealingly connected in open
fluid communication with a permeate-discharging face of each of said headers; and,
means to withdraw said permeate;
the improvement comprising.
said fibers, said headers and said permeate collection means together forming a
vertical skein wherein said fibers are essentially vertically disposed and terminal end
portions of individual fibers are potted in proximately spaced-apart relationship in cured
resin;
said first header being upper and disposed in vertically spaced-apart relationship
above said second header, with opposed faces at a fixed distance;
each of said fibers having substantially the same length, said length being from
between 0.1% to less than 5% greater than said fixed distance so as to permit restricted

displacement of an intermediate portion of each fiber, independently of the movement of
another fiber; and,
a gas distribution system having through-passages adapted to discharge bubbles
near to rise through or around the skein of fibers, the gas distribution system including
one or more gas tubes which space the first and second headers apart and which also
carry air to the through-passages.
25. (Amended) In a microfiltration membrane device, for withdrawing permeate
essentially continuously from a multi-component liquid substrate while increasing the
concentration of particulate material therein, said membrane device including:
a multiplicity of hollow fiber membranes, or fibers, unconfined in a shell of a
module, said fibers together having a surface area > 1 m ² , said fibers being swayable in
said substrate, said fibers being subject to a transmembrane pressure differential in the
range from about 0.7 kPa (0.1 psi) to about 345 kPa (50 psi), and each fiber having
length > 0.5 meter;
a first header and a second header disposed in transversely spaced-apart
relationship with said second header within said substrate;
a first header and a second header having opposed terminal end portions of
each fiber sealingly secured therein, all open ends of said fibbers extending from a
permeate-discharging face of at least one header;
permeate-collection means to collect said permeate, sealingly connected in open
fluid communication with a permeate-discharging face of each of said headers; and,
means to withdraw said permeate;
the improvement comprising,
said fibers, said headers and said permeate collection means together forming a
vertical skein wherein said fibers are essentially vertically disposed and terminal end
portions of individual fibers are potted in proximately spaced-apart relationship in cured
resin;
said first header being upper and disposed in vertically spaced-apart relationship
above said second header, with opposed faces at a fixed distance;

between 0.1% to less than 5% greater than said fixed distance so as to permit restricted displacement of an intermediate portion of each fiber, independently of the movement of
displacement of an intermediate portion of each fiber, independently of the movement of
and the first th
another fiber, wherein the headers are rectangular in plan view and the skein has about
30 or less arrays of fibers.
26. (Amended) A device for withdrawing permeate from a multicomponent liquid
substrate comprising.
(a) a reservoir under essentially ambient pressure having a feed zone for
containing a substrate;
(b) a microfiltration membrane device, for withdrawing permeate essentially
continuously from the multi-component liquid substrate while increasing the
concentration of particulate material therein, said membrane device including:
a multiplicity of hollow fiber membranes, or fibers, unconfined in a shell of a
module, said fibers together having a surface area > 1 m2, said fibers being swayable in
said substrate, said fibers being subject to a transmembrane pressure differential in the
range from about 0.7 kPa (0.1 psi) to about 345 kPa (50 psi), and each fiber having
<u>length > 0.5 meter;</u>
a first header and a second header disposed in transversely spaced-apart
relationship with said second header within said substrate;
a first header and a second header having opposed terminal end portions of
each fiber sealingly secured therein, all open ends of said fibers extending from a
permeate-discharging face of at least one header;
permeate-collection means to collect said permeate, sealingly connected in open
fluid communication with a permeate-discharging\face of each of said headers; and,
means to withdraw said permeate;
said fibers, said headers and said permeate collection means together forming a
vertical skein wherein said fibers are essentially vertically disposed and terminal end
portions of individual fibers are potted in proximately spaced-apart relationship in cured
resin;

said first header being upper and disposed in vertically spaced-apart relationship
above said second header, with opposed faces at a fixed distance;
each of said fibers having substantially the same length, said length being from
between 0.1% to less than 5% greater than said fixed distance so as to permit restricted
displacement of an intermediate portion of each fiber, independently of the movement of
another fiber,
the outside of the membranes in fluid communication with the feed zone of the
reservoir;
(c) a pump in fluid communication with the insides of the membranes through
the permeate collection means, the pump operable to supply a suction to the lumens of
the hollow fiber membranes to draw permeate through the membranes; and,
(d) a gas distribution means including a plurality of through-passages for
discharging bubbles which rise and contact fibers.
29. (Amended) In a microfiltration membrane device, for withdrawing permeate
essentially continuously from a multi-component liquid substrate while increasing the
concentration of particulate material therein, said membrane device including:
a multiplicity of hollow fiber membranes, or fibers, unconfined in a shell of a
module, said fibers together having a surface area >1 m², said fibers being swayable in
said substrate, said fibers being subject to a transmembrane pressure differential in the
range from about 0.7 kPa (0.1 psi) to about 345 kPa (50 psi), and each fiber having
length > 0.5 meter;
a first header and a second header disposed in transversely spaced-apart
relationship with said second header within said substrate;
a first header and a second header having opposed terminal end portions of
each fiber sealingly secured therein, all open ends of said fibers extending from a
permeate-discharging face of at least one header;
permeate-collection means to collect said permeate, sealingly connected in open
fluid communication with a permeate-discharging face of each of said headers; and,
means to withdraw the permeate;
the improvement comprising.

said fibers, said headers and said permeate collection means together forming a
vertical skêin wherein said fibers are essentially vertically disposed and terminal end
portions of individual fibers are potted in proximately spaced-apart relationship in cured
resin;
said first header being upper and disposed in vertically spaced-apart relationship
above said second header, with opposed faces at a fixed distance:
each of said fibers having substantially the same length, said length being from
between 0.1% to less than 5% greater than said fixed distance so as to permit restricted
displacement of an intermediate portion of each fiber, independently of the movement of
another fiber;
walls extending downwards from a lower header of the first and second header,
the walls being adapted to retain a gas below the lower header; and,
through-passages for gas to pass through the lower header from an area below
the lower header bordered by the walls